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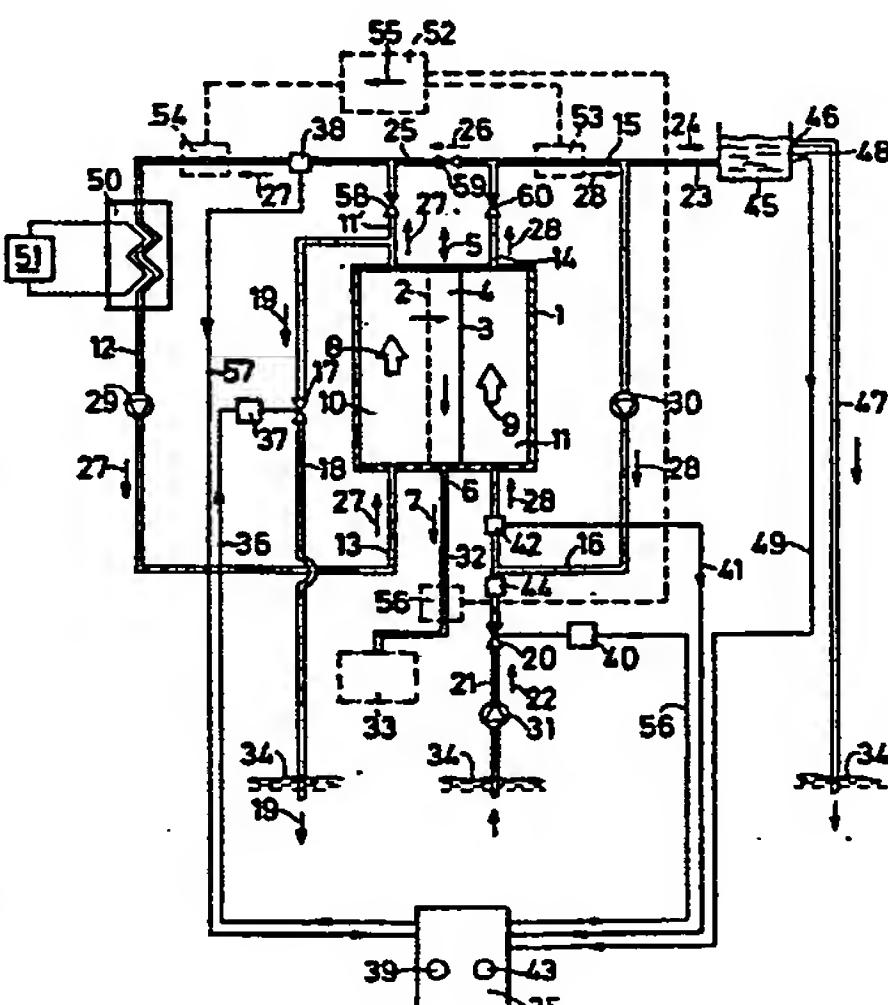
INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 4 :		A1	(11) International Publication Number:	WO 87/00160
C02F 1/04			(43) International Publication Date:	15 January 1987 (15.01.87)
(21) International Application Number:	PCT/SE86/00290		(81) Designated States:	AU, BR, CH (European patent), DE (European patent), DK, FI, FR (European patent), GB (European patent), IT (European patent), JP, NO, SU, US.
(22) International Filing Date:	16 June 1986 (16.06.86)			
(31) Priority Application Number:	8503335-5		Published	
(32) Priority Date:	4 July 1985 (04.07.85)			<i>With international search report.</i>
(33) Priority Country:	SE			
(71) Applicant (for all designated States except US):	SVENSKA UTVECKLINGS AB [SE/SE]; Box 27304, S-102 54 Stockholm (SE).			
(72) Inventors; and				
(75) Inventors/Applicants (for US only) :	KJELLANDER, Nils [SE/SE]; Hagavägen 10, S-171 53 Solna (SE). RODESJÖ, Bo [SE/SE]; Ingefasts väg 85, S-183 42 Täby (SE).			
(74) Agent:	ÖRTENBLAD, Bertil; Noréns Patentbyrå AB, Banérsgatan 73, S-115 26 Stockholm (SE).			

(54) Title: APPARATUS FOR DESALINATING SALT WATER BY MEMBRANE DISTILLATION

(57) Abstract

An apparatus for desalinating sea water, comprising a distillation unit which includes a porous hydrophobic membrane which is pervious to steam but impervious to water, and a condensation surface arranged at a distance from the membrane, the distillation arrangement also including a first unit for heating and conducting the water to be distilled on one side of the membrane, and a second unit arranged to conduct a liquid which is colder than the water, on the side of the condensation surface remote from the membrane, distilled water being collected and drawn-off between the membrane and the condensation surface. The apparatus is characterized in that the first unit incorporates a closed pipe loop (11, 12, 13) which is connected in series with the warm side (10) of the distillation unit (1); in that the second unit incorporates a closed pipe loop (14, 15, 16) which is connected in series with the cold side (11) of the distillation unit (1); in that a drainage valve (17) is provided for drawing-off water from the pipe loop (11, 12, 13), of the first unit; in that there is provided a water filling valve (20) and a pipe line (23) for drawing water from the pipe loop (14, 15, 16) of the second unit; in that the pipe loops of respective first and second units are connected together by means of a connecting line (25); and in that a heat exchanger (50) is connected to the pipe loop (11, 12, 13) of the first unit for supplying energy to the water present in the pipe loop of the first unit.



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Apparatus for desalinating salt water by
membrane distillation

The present invention relates to an apparatus for de-salinating salt water by membrane distillation.

- Apparatus utilizing membrane distillation are known to
5 the art, inter alia from the Swedish Patent Specification
No. 419 699. The Swedish patent specification describes
an apparatus for membrane distillation comprising a plura-
lity of first cassettes for conducting warm salt water and
a plurality of second cassettes for conducting a cold
10 liquid, such as cold sea water. Located between each pair
of mutually adjacent cassettes is a separation cassette
which separates one of the first cassettes from one of
the second cassettes.
- 15 The separation cassette according to the aforesaid Patent
Specification includes a hydrophobic porous membrane
which constitutes one side surface of the cassette, and
a thin plastics film which constitutes the other side
surface of the cassette, the membrane being spaced from
20 the plastic film so as to form an air gap between the
membrane and the film. Warm salt water flows towards the
membrane from the side thereof remote from the air gap
and enters one of the first cassettes, whereas cold water
flows into one of the second cassettes on the side of the
25 plastic film remote from said air gap.
- Distillation is effected in a manner such that the hot
or warm salt water gives off water vapour which passes
through the pores of the membrane and through said air
gap, whereafter the water vapour condenses on the cold
30 plastic film. The pores should be of a size which pre-
vents liquid water from passing therethrough.
- Such a distillation process affords a number of advan-
35 tages; for example the process takes place at a temperature

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beneath the boiling point of water and approximately at atmospheric pressure, which enables a non-corrosive construction material to be used. In addition, such a process is relatively highly productive in relation to 5 the size of the cassettes and the numbers thereof.

However, the process is encumbered with one serious disadvantage. This disadvantage is based on the fact that 10 large quantities of energy are transported from the hot salt water on the evaporation side to the cold water on the condensation side for each product water-unit desalinated.

This energy transport results in a lowering of the temperature of the hot water flow and a corresponding increase in temperature of the cold water flow. Lowering of 15 the temperature in the hot water flow and also the decrease in the temperature gap between the hot and the cold flow decreases the production of fresh water. In 20 order to maintain an acceptable level of productivity, it is necessary to restrict these changes in temperature.

This can only be achieved by increasing the flows of 25 heated salt water and cold water respectively through the desalinating unit.

This means that large quantities of salt water must be heated. In addition, large quantities of cooling water must be pumped through the distillation unit.

30 In order for such a process to function satisfactorily the water supplied to the process must be pre-treated by filtration and chemical treatment. Thus, the use of large quantities of water necessitates expensive heating and expensive treatment processes.

35 The present invention solves this problem, so that solely minor quantities of cold sea water supplied to the system need be heated and minor quantities of cold salt

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water need be supplied for cooling purposes, at the same time as a significant part of the energy transferred from the hot salt water to the cold salt water is recovered.

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The invention also enables the process to be readily controlled.

Thus, the present invention relates to an apparatus for desalinating salt water, comprising a distillation unit which includes a porous, hydrophobic membrane which is pervious to steam or water vapour but is impervious to water, and a condensation surface arranged at a distance from the membrane, said distillation unit further comprising a first unit for heating water to be distilled and conducting said water on one side of the membrane, and a second unit arranged to conduct a liquid, which is colder than said water, on the side of the condensation surface remote from the membrane, distilled water being collected and drawn off between said membrane and said condensation surface, the invention being characterized in that said first unit includes a closed pipe loop which is connected in series with the warm side of the distillation unit; in that said second unit includes a closed pipe loop connected in series with the cold side of the distillation unit; in that there is provided a drainage valve for drawing off water from the loop of the first unit; in that there is also provided a water-filling valve and a pipeline for drawing water from the loop of the second unit; and in that the loops of the first and the second units are connected together by means of a connecting line; and in that a heat exchanger or the like is connected to the loop of the first unit for supplying energy to the water present in said loop.

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The invention will now be described in more detail with reference to an exemplifying embodiment thereof illustrated in the accompanying drawing, the single Figure of

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which is a schematic flow diagram of an apparatus according to the invention.

- Figure 1 illustrates schematically and in cross-section a distillation unit 1 which includes the aforesaid cassettes and comprises a porous hydrophobic membrane 2 which is permeable to steam or water vapour but impermeable to liquid, and further comprises a condensation surface in the form of a plastic film 3 located at a distance from the membrane. Located between the membrane 2 and the plastic film 3 is an air gap 4 which incorporates a channel or the like for communication with the atmosphere as illustrated by the arrow 5. Arranged at the lower end of the air gap 4 is a channel 6 or the like for conducting away fresh water-condensate from the air gap, as illustrated by the arrow 7. The membrane 2 and the plastic film 3 may be suspended from any suitable construction.
- Arranged on one side of the unit 1 is a first chamber 10 for conducting the liquid to be distilled, as illustrated by the arrow 8, so that the liquid covers the side of the membrane remote from the air gap.
- Arranged on the other side of the unit 1 is a second chamber 11 for conducting a liquid which is colder than the liquid to be distilled, as illustrated by the arrow 9, so that the colder liquid covers the side of the plastic film remote from the air gap.
- According to the invention the first unit incorporates a closed first pipe loop 11,12,13 which is connected in series to the first chamber 10 of the distillation unit. The second unit also incorporates a closed, second pipe loop 14,15,16, which is connected in series with the second chamber 11 of the distillation unit.

The illustrated apparatus also includes a drainage valve

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17 for drawing water from the pipe loop 11,12,13 of the first unit, in the direction shown by the arrows 19. A pipe 18 extends from the closed loop 11,12,13 to a drain, via the drainage valve 17.

5

A filling valve 20 for filling the loop 14,15,16 of the second unit with water is mounted on a pipe 21 intended for supplying sea water at normal seawater temperature in the direction of the arrow 22, the pipe 21 being connected to the pipe loop 14,15,16 of the second unit.

10

Also extending from the pipe loop 14,15,16 of the second unit is a pipe 23 for drawing water from the pipe loop of the second unit in the direction shown by the arrow 24.

15

The pipe loops of the two units are connected together at a location thereon by means of a connecting line 25. When the apparatus is operating, water is transferred intermittently or continuously through the connecting line 25 from the second unit to the first unit, as illustrated by the broken arrow 26. The arrows 8, 27 illustrate the flow direction in the first pipe line 11,12,13, whereas the arrows 9, 28 illustrate the flow direction in the second pipe loop 14,15,16.

20

Each pipe loop incorporates a respective pump 29,30 for advancing the water through respective loops. A pump 31 is provided for pumping sea water into the second pipe loop, via the pipe 21.

25

30 The distilled water produced is carried away through a pipe 32, to a collecting vessel 33 or to a consumer.

30

35 Each distillation apparatus normally comprises a very large number of distillation units 1 connected together in parallel, although only one such unit has been shown in Figure 1 for the sake of clarity.

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As will be understood, the volumetric capacity of the collecting vessel 33 in relation to the distillation unit 1 is much greater than that illustrated in the Figure.

- 5 In the Figure! the reference 34 identifies the surface of the sea, although it will be understood that the apparatus can be placed at some other location other than in the immediate proximity of the sea water.
- 10 According to the invention the drainage valve 17 is controlled by means of a control device 35, via an electric conductor 36. The valve 17 is suitably a magnetic valve, i.e. a valve controlled by an electromagnetic device 37. The control device 35 is arranged to control the valve 17 in response to a signal emanating from a transducer 38 in the form of a salinometer of a kind known per se. The signal is relayed on an electric conductor 57. This signal constitutes a real-value signal. The control device 35 incorporates a setting means 39, for example in the form of a potentiometer, for setting a control value, or a control value interval.

When the water present in the first loop 11,12,13 is distilled, steam is transported through the membrane 2, causing the salt content in the loop to rise. In conjunction herewith the control device 35 receives a signal from the salinometer 38; indicating an increase in salt content. The control device 35 is arranged herewith to cause the drainage valve 17 to open the connection between the first pipe loop and the free atmosphere, in Figure 1 illustrated by the sea-water surface 34. Introduction of further water is effected from the second pipe loop 14,15,16, via the aforementioned connecting line 25, synchronously with draining water through the pipe-line 18. Since the salt content of the water in the second pipe loop is lower than the elevated salt content of the first pipe loop the salt content of the first pipe loop will fall when introducing further water

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thereinto. The control device 35 is arranged to close the valve 17 when the salt content has fallen to a pre-determined level set through the setting means.

5 Thus, the first loop is filled solely with water from the second pipe loop, through the single connecting line or pipe 25 between the two loops.

10 The apparatus as a whole is replenished with water solely through the aforementioned filling valve 20, i.e. to the second pipe loop 14,15,16. The filling valve 20 is also controlled by an electromagnetic device 40, i.e. a magnetic valve. The filling valve 20 is controlled by means of 15 a control device 35, which is preferably the same device as that which controls the drainage valve 17, but which may also be a separate control device.

The control device controls the filling valve via an electric conductor 56.

20 The control device 35 is arranged to control the introduction of water to the second pipe loop 14,15,16 in response to a signal transmitted from a temperature sensor 42 over an electric conductor 41, in a manner to maintain a 25 pre-determined temperature in the pipe loop of the second unit.

This signal constitutes a real-value signal. The control device 35 incorporates a setting means 43, for example 30 in the form of a potentiometer, for setting a control value or a control value interval.

In order to obtain effective distillation, it is necessary for a temperature difference to prevail between the two 35 pipe loops of respective units. By filling the apparatus with water through the filling valve 20, either intermittently or continuously, at the same time as the amount of water introduced is substantially less than the

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flow in the pipe loop 14,15,16, a sufficiently low temperature is maintained in the second unit without needing to supply the second unit continuously with large quantities of water. Thus, far less water need be filtered and treated with chemicals than when the quantity of water introduced into the second unit is equal to the flow in the said second unit. A filtering and chemical-treatment stage 44 is illustrated schematically in the Figure.

10

Since a pre-determined lower temperature is to be maintained in the second unit, however, it is necessary for the amount of water introduced via the filling valve to exceed the amount of water transferred to the first pipe loop via the connecting pipe 25, unless a separate cooling device is incorporated in the pipe loop of the second unit. In view of this, the aforesaid pipe 23 is provided for the purpose of taking water from the second pipe loop.

15

According to one preferred embodiment of the invention, the aforesaid pipe 23 extends via a vessel 45 provided with a spillway 46, from which a pipe 47 extends into the sea or ocean 34.

20

In accordance with the invention, the volumetric capacity of the vessel 45 is sufficient to replace the volume taken from the first unit at one and the same point in time via the drainage valve 17. In this way it is not necessary to synchronize drawing of water from the first unit with corresponding filling of the second unit with water via the filling valve 20. According to one embodiment, the vessel 45 is provided with a level sensor 48, which is arranged to send a first electric signal to the control device 35 over a conductor 49 when the level of water in the vessel has fallen to a pre-determined value. When this pre-determined level is reached, the control device 35 causes the filling valve 20 to open, and holds

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the valve in its open mode until the level sensor 48 sends a second signal to the control device 35, this second signal signifying that the level has been restored to a pre-determined level.

5

According to a further, preferred alternative embodiment, however, the control device 35 is adapted to open the filling valve 20 at the same time as the aforesaid drainage valve 17 is opened, so that water is introduced 10 synchronously into the second unit when water is transferred to the first unit via the connecting pipe 25.

In order to obtain the requisite water temperature in 15 the first unit, the water passes a heat exchanger connected to an energy source 51.

Although the energy source 51 may be any suitable source, it preferably comprises a source of waste heat. For example, the heat source may comprise the cooling water 20 system of a diesel engine used to produce electrical energy for driving the aforesaid pumps and control devices. In those countries which enjoy a warmer climate solar panels may be used, either separately or in combination with a waste-heat source. When there is adequate 25 access to electrical energy, the energy source 51 may comprise a source of electrical energy.

One characteristic of a membrane distillation process according to the aforementioned Swedish Patent is that 30 the flow through the membrane 2 greatly increases progressively with increasing temperature of the water to be distilled. In this case, the cooling water in the second unit is assumed to be held at a substantially constant level.

35

When applied to the present invention, this means that the process becomes self-regulating such that the process itself finds its own working level, due to the fact that

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the amount of water distilled in the first unit corresponds to the amount of energy supplied, wherewith a corresponding amount of pre-heated water is also supplied to the pipe loop of the first unit from the pipe loop

5 of the second unit, via the connecting pipe. The supply of water to the pipe loop of the second unit for maintaining the aforesaid pre-determined temperature therein is also directly dependent on the amount of water distilled.

10 By way of example it can be mentioned that when the water in the first unit has a temperature of 80°C and the water in the second unit is permitted to have a temperature of 60°C, the relationship between the flows in the process is as follows:

15 Quantity of distilled water via the pipe 32; quantity of water drawn from the second unit via the pipe 23; quantity of water drawn from the first unit via the pipe
 $18 = 1:10:2$.

20 Those energy losses occurring in a process of this kind are primarily due to heat transport through the membrane
2. Owing to the fact that a separate cooling loop is provided, mainly the second pipe loop, a significant
25 part of these energy losses is recovered by heating the water in the loop. Since this water is transferred to the first pipe loop, the first unit is therefore supplied with pre-heated water.

30 As will be clearly seen from the aforesgoing, the present invention solves the aforesaid problems regarding the large quantities of water needing to be filtered, treated with chemicals and heated. In addition, a significant part of the energy transported through the membrane is recovered. The apparatus also finds its own working level in dependence on the energy supplied.

In order to further improve the efficiency of the apparatus and reduce the amount of water which need be supp-

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lied, there is provided in accordance with a preferred embodiment a heating arrangement comprising a heat pump 52 of a known kind. The evaporator 53 of the heat pump 52 is connected to the second pipe loop via a heat exchanger,

5 and the condenser 54 of said heat pump is connected to the first pipe loop via a heat exchanger. Thus, energy is transferred via the heat pump from the second unit to the first unit, as illustrated by the arrow 55.

10 According to a modified embodiment, the heat pump includes a further evaporator 56 connected, via a heat exchanger, to the pipe 6 through which distilled water is removed from the apparatus. This enables part of the heat content of the distilled water to be recovered.

15 By using a heat pump in the aforescribed manner, substantially all energy lost from the distillation process is recovered.

20 The reference numerals 58,59,60 in the Figure identify one-way valves which permit water to flow in solely one direction, from the non-filled side to the filled side of the valve.

25 In the aforesgoing, the invention has been described with reference to one embodiment thereof. It will be understood, however, that modifications can be made to the illustrated embodiment. For example, the illustrated components can be replaced with other components having 30 an equivalent function, and the schematically illustrated coupling diagram of the pipe system illustrated in the Figure can be modified without departing from the concept of the invention, namely the arrangement of a first unit in which the warm water flows in a loop, the arrangement of a second unit in which the cold water flows in a loop, and the joining of the loops so that the first unit is filled by taking water from the second unit.

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Thus, the present invention is not restricted to the
aforedescribed and illustrated embodiment, and modifica-
tions can be made within the scope of the following
Claims.

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CLAIMS

1. Apparatus for desalinating salt water, comprising a distillation unit which incorporates a porous hydrophobic membrane which is pervious to steam but impervious to water, and further incorporating a condensation surface arranged at a distance from the membrane, said distillation arrangement further including a first unit for heating and conducting the water to be distilled on one side of the membrane, and a second unit arranged to conduct water which is colder than the first mentioned water, on the side of the condensation surface remote from the membrane, distilled water being collected and drawn-off between said membrane and said condensation surface, characterized in that said first unit includes a closed pipe loop (11,12,13) which is connected in series with the warm side (10) of the distillation unit (1); in that said second unit includes a closed pipe loop (14,15,16) which is connected in series with the cold side (11) of the distillation unit (1); in that there is provided a drainage valve (17) for drawing water from the pipe loop (11,12,13) of the first unit; in that there is provided a filling valve (20) for filling with water, and a pipe line (23) for drawing water from the pipe loop (14,15,16) of the second unit; in that the respective pipe loops of the first and the second units are connected together by means of a connecting line (25); and in that a heat exchanger (50) or the like is connected to the pipe loop (11,12,13) of the first unit for supplying energy to the water present in the pipe loop of the first unit.
2. Apparatus according to Claim 1, characterized in that the drainage valve (17) is controlled by means of a control device (35) arranged to control the withdrawal of water in response to a signal from a salinometer (38) incorporated in the pipe loop (11,12,13) of the first unit, so as to maintain a pre-determined salt content in the pipe loop (11,12,13) of the first unit.

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3. Apparatus according to Claim 2, characterized in that the filling valve (20) is controlled by means of a control device (35) arranged to control a filling operation in response to a signal from a temperature sensor (42)

5 in a manner to maintain a pre-determined temperature in the pipe loop (14,15,16) of the second unit.

4. Apparatus according to Claim 2 and 3, characterized in that said control device (35) is arranged to open the

10 filling valve (20) at the same time as the drainage valve (17) is opened.

5. Apparatus according to Claim 1,2,3 or 4, characterized in that the pipe line (23) of the second unit extends via

15 a vessel (45) provided with a spillway (46).

6. Apparatus according to Claim 1,2,3,4 or 5, characterized in that the first unit has a heating arrangement which comprises a heat pump (52), the evaporator (53) of which

20 is connected to the pipe loop (14,15,16) of the second unit, and the condenser (54) of which is connected to the pipe loop (11,12,13) of the first unit.

7. Apparatus according to Claim 6, characterized in that

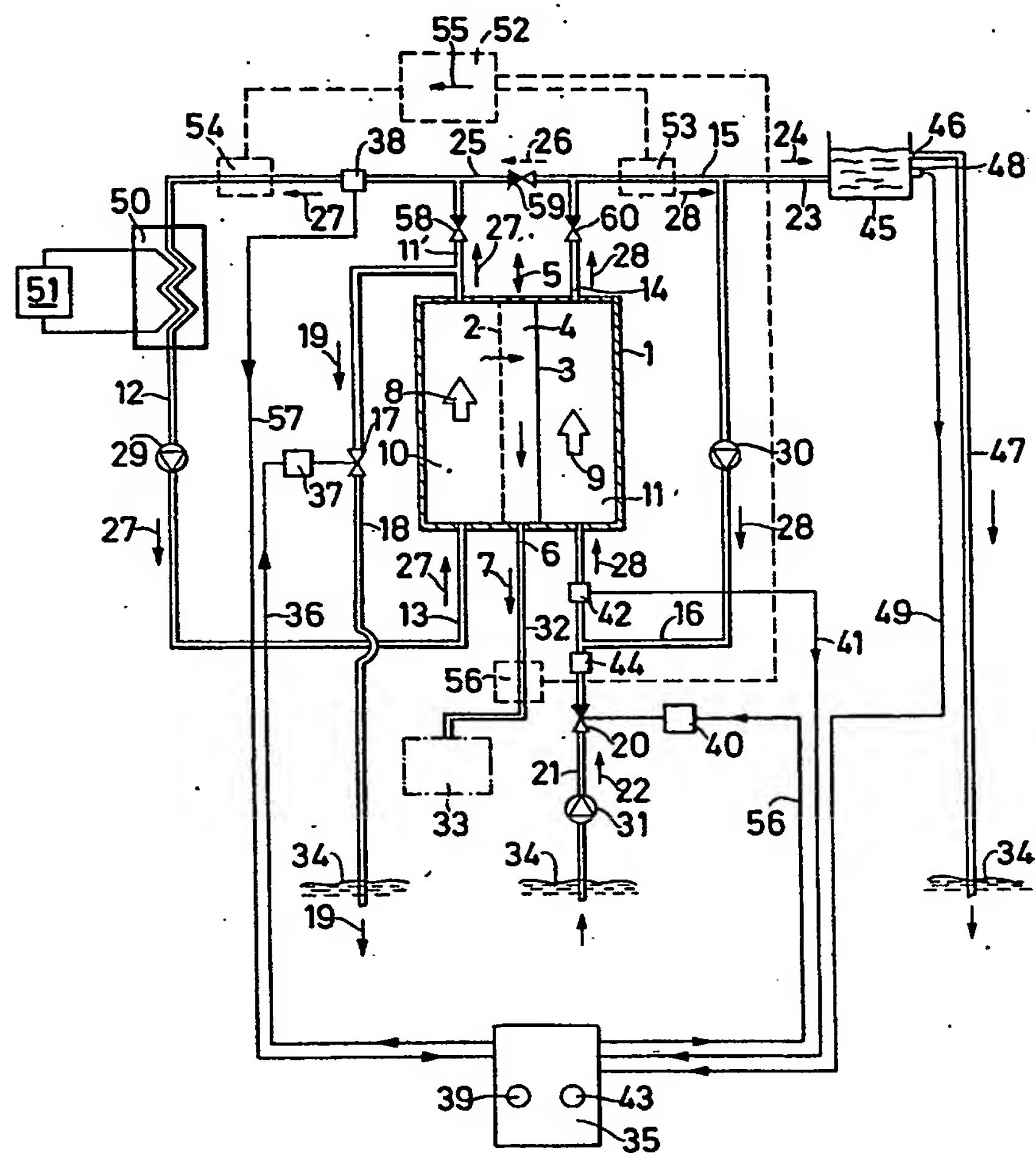
25 the heat pump (52) includes a further evaporator (56) which is connected to a pipe (6) for drawing-off distilled water.

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Fig. 1



INTERNATIONAL SEARCH REPORT

International Application No PCT/SE86/00290

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) *		
According to International Patent Classification (IPC) or to both National Classification and IPC 4		
C 02 F 1/04		
II. FIELDS SEARCHED		
Minimum Documentation Searched †		
Classification System	Classification Symbols	
IPC 4 US CL	C 02 F 1/04, /08, /14, /18; B 01 D 13/00 <u>203</u> : 10, 11	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched §		
SE, NO, DK, FI classes as above		
III. DOCUMENTS CONSIDERED TO BE RELEVANT*		
Category *	Citation of Document, ** with indication, where appropriate, of the relevant passages ††	Relevant to Claim No. 13
A	SE, A, 8 403 081 (SVENSKA UTVECKLINGS AB) 8 December 1985	1
A	EP, A, 0 039 197 (W L GORE & ASSOCIATES, INC) 4 November 1981	1
A	Chemical Abstracts, Vol 70 (1969) abstract No 070972	
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IV. CERTIFICATION		
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